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Application of X-ray micro-computed tomography on high-speed cavitating diesel fuel flows

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Abstract The flow inside a purpose built enlarged single-orifice nozzle replica is quantified using time-averaged X-ray micro-computed tomography (micro-CT) and high-speed shadowgraphy. Results have been obtained at Reynolds and cavitation numbers similar to those of real-size injectors. Good agreement for the cavitation extent inside the orifice is found between the micro-CT and the corresponding temporal mean 2D cavitation image, as captured by the high-speed camera. However, the internal 3D structure of the developing cavitation cloud reveals a hollow vapour cloud ring formed at the hole entrance and extending only at the lower part of the hole due to the asymmetric flow entry. Moreover, the cavitation volume fraction exhibits a significant gradient along the orifice volume. The cavitation number and the needle valve lift seem to be the most influential operating parameters, while the Reynolds number seems to have only small effect for the range of values tested. Overall, the study demonstrates that use of micro-CT can be a reliable tool for cavitation in nozzle orifices operating under nominal steady-state conditions.

1 Introduction

The ever more stringent emission regulations of direct-injection diesel engines, imposed by the regulatory boards worldwide, have triggered the race of improving the

efficiency of such engines. Among others, the fuel injection equipment (FIE) is a key component for improving the efficiency of environmentally friendly engines. Recent advances dictate the use of extra high injection pressures, of the order of 3000 bar and tiny flow passages (injection holes) of the order of 100–250 μm in diameter, for improved fuel atomisation and combustion efficiency. Under these circumstances, cavitation has been found to develop inside fuel injection nozzles at the early studies of Badock et al. (1999), Bergwerk (1959), Chaves et al. (1995) and Nurick (1976), followed by Arcoumanis et al. (2000), Blessing et al. (2003), Mitroglou et al. (2014) and Roth et al. (2002) in more realistic real-size nozzle geometries offering optical access; equally helpful studies performed in transparent enlarged nozzle replicas [selectively (Andriotis et al. 2008; Arcoumanis et al. 2000; Miranda et al. 2003; Mitroglou and Gavaises 2013; Powell et al. 2000)] also indicate that cavitation plays an increasingly significant role in the nozzle's internal flow structure and development. Cavitation inside an injection hole is believed to enhance spray atomisation, either directly through the implosion of cavitation bubbles or indirectly because it increases turbulence in the nozzle flow (Badock et al. 1999; Walther 2002); unfortunately, under certain circumstances induces erosion (Dular and Petkovšek 2015; Koukouvinis et al. 2016) that may lead to catastrophic failures. Moreover, cavitation inside the injection holes promotes shot-to-shot spray instabilities (Mitroglou et al. 2011, 2012; Suh and Lee 2008), which, in turn, are responsible for poor combustion efficiency and increased emissions (Hayashi et al. 2013). Two distinct macroscopic forms of cavitation have been identified, which are referred to as geometry-induced and vortex or 'string' cavitation. The former can be, partially or totally, suppressed by appropriate design of the inlet hole curvature and non-cylindrical injection hole

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shape (Soteriou et al. 2006), for sufficiently high positions of the needle valve (i.e. open); this is now the standard practice in manufacturing automotive diesel injector nozzles (Pötz et al. 2000); still, some cavitation may be needed as it is thought to make nozzles more resistant against deposit formation (Tang et al. 2009). Cavitation is also known to decrease the nozzle flow rate (Soteriou et al. 1995) and lead in some cases (but not always) to flow choking (Payri et al. 2006). On the other hand, vortex-induced cavitation and turbulent flow in a fuel injector nozzle may lead to complex structures which remain not well-understood.

Nozzle cavitation has been traditionally studied using visualisation techniques; in some of the relevant early studies, parts of a nozzle were replaced with transparent replicas (i.e. single injection hole), allowing unobstructed visible access (Chaves et al. 1995; Roth et al. 2005; Winkelhofer et al. 2001). Many investigations have been performed on transparent, enlarged full nozzle replicas; due to the significantly lower injection pressures utilised in such enlarged models (Gavaises et al. 2009; Mitroglou and Gavaises 2013; Soteriou et al. 2006), dimensionless similarity based on the cavitation (CN) and Reynolds (Re) numbers has been adopted. Parallel to those activities, attempts were also made to manufacture real-size exact replicas of diesel nozzles from transparent materials that are able of withstanding pressures in the range of 500–2000 bar, which are similar to those in real injections. Such successful studies have been presented in Blessing et al. (2003), Hayashi et al. (2013), Jollet et al. (2013), Mitroglou et al. (2011, 2014) and Reid et al. (2010, 2014) and have confirmed the observations reported from the enlarged transparent models. In most cases, there is evidence of the interrelated geometric-induced and vortex cavitation. Moreover, string cavitation owes its existence either to vortices that cavitate or to sources of vapour, or pre-existing nuclei inside the nozzle that grow when trapped inside flow vortices. All observations so far have confirmed that the developed multi-phase flow field is complex and exhibits a transient behaviour, even at simplified single-orifice geometries.

High-speed visualisation applied on all aforementioned investigations have succeeded in capturing in detail the transient flow behaviour; however, they exhibit certain drawbacks due to the fact that light scatters and refracts strongly on liquid–vapour interfaces present inside the flow channel. Single scattering, and more severely multiple scattering, reduces, or totally blocks, light transmission, even at very low vapour fractions; the latter degrades the ability of optical techniques to provide quantitative measurements of fluid density, especially in optically dense multiphase flow fields and even increases the uncertainty of the produced qualitative representations.

Despite the opacity of multiphase flow systems, quantitative experiments are necessary for the deeper understanding

of the flow physics; in this direction, several research groups worldwide have developed other non-invasive measurement techniques. As stated in Dudukovic (2000), a multiphase flow experimental system should have: (1) high spatial and temporal resolution for local phase fraction measurements, as well as velocity field measurements of all phases, and (2) the capability to provide instantaneous and time history snapshots of the flow. Note, however, that a single experimental system that can satisfy all these needs does not currently exist (Heindel 2011). Despite the recent advances in laser diagnostics, such as ballistic imaging or structured illumination to mitigate the multiple scattering effects (Berrocal et al. 2008; Linne et al. 2006), their ability to measure fluid density is still limited (Leick et al. 2011). Moreover, flows with significant refractive index gradients, such as liquid diesel and vapour, exhibit beam-steering effects that interfere with optical diagnostics by creating uncertainty in the location of the volume under observation (Heindel 2011). Invasive measurement techniques, such as probes, interfere and alter the internal flow field that is under investigation and thus, they cannot be used with the small orifices utilised with fuel injection equipment.

Multiple non-invasive quantitative flow visualisation techniques have been reviewed in the literature over the years (Chaouki et al. 1997; Dudukovic 2000; Duke 2015; Heindel 2011; Kastengren and Powell 2014; Yates et al. 2002). One of the first applications of X-ray imaging for visualisation of air bubbles in gas–solid fluidised beds was performed in the 1950s and 1960s (Grohse 1955; Rowe and Partridge 1997). A variety of tomographic, or 2-D radiographic, X-ray techniques have been developed, where tomography refers to the cross-sectional imaging of a system from either transmission or reflection data collected by illumination of the flow system from many different angles (Kak and Slaney 2001), while radiography refers to single-angle collection data. In X-ray tomography, unlike soft-field methods (Marashdeh et al. 2008), the field lines of the measured property (e.g., X-ray attenuation) are not influenced by material density changes outside the path of a single X-ray. The latter simplifies reconstruction; however, due to the current technology of detection systems and X-ray source flux, data acquisition is typically slow, in relation to cavitation time-scales, for a laboratory-scale micro-tomography facility. On the contrary, synchrotron X-ray sources provide a far greater degree of brilliance than laboratory-scale sources, permitting a much greater scope for advanced X-ray diagnostics. Synchrotron sources have existed for many years, but have until recently found relatively little usage by the fuel injection community (Duke et al. 2013, 2014, 2015a; Kastengren et al. 2012; Moon et al. 2015; Powell et al. 2000; Wang et al. 2008). Nevertheless, laboratory-scale X-ray sources have improved characteristics in recent years, featuring small spot-sizes,

which if coupled with developments in detector technology, provide adequate spatial resolution for multiphase flow applications.

One of the first attempts to apply X-ray CT measurements on multiphase flows is dated back at 1983 (Ikeda et al. 1983); the technique was applied on a steady-state U-shaped tube air–water flow system. Measured void fractions were compared against results of intrusive techniques and demonstrated good agreement. Recent examples of application of X-ray techniques on cavitating flows are found in Coutier-Delgosha et al. (2006) and Stutz and Legoupil (2003); tube source X-rays, with relatively low photon fluxes, have been used to provide vapour volume fraction measurements of sheet cavitation over a hydrofoil inside a two-dimensional channel flow. Additionally, recent investigations on cavitating flow inside cylindrical flow channels is found in Bauer et al. (2012); a medical CT scanner was utilised for providing measurements inside an enlarged cavitating pipe flow ($D = 20$ mm) using water as the working fluid. The reconstructed void fraction along the pipe length revealed the formation of water vapour at the channel walls, for the first half of the hole length (forming a liquid core), and also a weak vapour accumulation around the channel axis (core of the flow) at the second half of the channel length. The former, which had been observed previously using visualisation techniques, was an expected behaviour; however, the latter, which had not been captured by conventional visualisation techniques, was an unexpected flow feature not previously observed. Similarly, a highly tuned medical X-ray source was used in Ganesh et al. (2015), Mäkiharju et al. (2013) and Sun et al. (2015) to study cavitation in the wake of bluff bodies and two-dimensional wedges inside a water tunnel. As demonstrated, low void fraction regions in partial cavities could provide conditions necessary for the existence of bubbly shocks, which act as a dominant mechanism of shedding of partial cavities under certain conditions. The latter behaviour was verified using X-ray densitometry at frame rates reaching 1 kHz, an acquisition speed that enabled the capture of dynamics of bubbly shock fronts with and without the presence of an obstacle. Finally, time-resolved and mean X-ray densitometry-based vapour volume fraction of the span-wise and plan view (for the case of a 2-D wedge) averaged flow field have been related to the vortex dynamics in order to explain vapour production in such transient flow dynamics.

Tube source X-rays have a large wavelength spread and a divergent beam and can provide high spatial resolution over long acquisition times; time-resolved measurements can be obtained at reduced spatial resolution; however, it is difficult to satisfy both requirements simultaneously. Such problems are overcome by the use of focused synchrotron X-rays that offer an advantageous combination of temporal

and spatial resolution due to high photon flux; however, the main drawback is the limitation of focus in a relatively small area (Duke et al. 2013). Nevertheless, relevant studies have been performed in Battistoni et al. (2015) and Duke et al. (2013, 2014, 2015b), where multiphase flow inside a cavitating channel has been studied and compared to computational fluid dynamics (CFD) results. Researchers performed an X-ray radiography experiment on a model nozzle of 500 μm in diameter. They exploited raster scan radiography and achieved a spatial resolution of 5 μm and a temporal resolution of 3.6 μs . Their experimental test-rig was able of delivering high CN at low discharge pressures, and Re of the order of 15 k. Vapour structures were found to be relatively steady, as time-resolved measurements indicated that root-mean square (RMS) fluctuations did not exceed 1% of the mean values. The spectral content of cavitation was found to be concentrated at small Strouhal numbers, of the order of 0.001–0.1, suggesting steady cavitation inception and mixing processes without large-scale fluctuations. Extensive vapour regions at the nozzle centre-line, where cavitation is not expected to occur, were identified, similar to Bauer et al. (2012); however, the authors reported that this could be due to dissolved gas present in the fuel that comes out of solution if the static pressure at that region is low. Similar studies involving synchrotron sources have also been applied on dense, high-pressure diesel/gasoline sprays, as described in Moon et al. (2010, 2015), where an ultrafast X-ray imaging technique has been applied. All recent advances in synchrotron X-rays and relevant imaging techniques are well described in Duke et al. (2015a, b), Duke (2015) and Kastengren and Powell (2014).

The present investigation exploits the increased spatial resolution of a cone-beam CT system (Santini et al. 2013) to quantitatively measure mean, three-dimensional vapour volume fraction inside a custom-design, scaled-up model channel flow that uses diesel as the working fluid. Due to the required long sampling times, the obtained mean vapour volume fractions are compared against ultra-high-speed flow visualisation results to qualitatively assess the dynamic behaviour of the flow. The study demonstrates the ability of a laboratory-scale X-ray source to provide the average, three-dimensional vapour volume fraction, and it is able to capture the effects of several flow parameters on cavitation structures present inside the custom injection hole.

2 Methods

The custom, purpose-built model features a non-symmetric flow arrangement that intends to mimic the flow patterns realised inside an orifice of a multi-hole diesel nozzle.

2.1 Nozzle geometry and high-pressure test-rig

As illustrated in Fig. 1, the nozzle comprises a single injection hole ($D = 3$ mm, $L = 9.5$ mm), whose axis is at an offset to the main axis of symmetry of the device. The achieved asymmetry, combined with the non-symmetric needle, ensures a flow field that promotes cavitation mainly on one side of the orifice entry, enabling unobstructed view of the cavitation pocket created from any angle. This configuration is similar to the single-hole, high-pressure transparent design presented by Reid et al. (2010), which has operated at pressures up to 2000 bar. As presented in this study, the observed flow field inside and upstream of the orifice has many similarities in cavitation development to that of multi-hole diesel nozzles. The test-rig has been designed specifically for use inside the micro-CT facility developed at the University of Bergamo (Fig. 1). The needle is set at a fixed position, while the pressure difference across the orifice is also constant during one experimental case; tested values ranged from 10 to 40 bar. The hydraulic unit that drives the system is a commercial one, able of delivering a maximum flow rate of 40 l/min. It was modified to accommodate a water–fuel heat exchanger equipped with a temperature control mechanism for accurate diesel fuel temperature control and monitor throughout the experimental campaign. The fuel temperature did not deviate more than 0.5 °C from the set-point that was 40 °C, regardless of the set pressure level (diesel properties at 40 °C: $\rho = 850$ kg/m³, $\nu \sim 3.9$ mm²/s). The conditions presented in this study are listed in Table 1.

The material of the nozzle was selected in order to enhance the X-ray signal to noise ratio. Various plastic and composite materials were evaluated that exhibit low X-ray attenuation, as opposed to metals; the polymer material PEEK (Polyether ether ketone) was selected, which exhibits low radiation attenuation and, at the same time, it has very appealing mechanical characteristics, necessary to withstand an inlet pressure of up to 55 bar and outlet pressure of up to 20 bar.

2.2 X-ray computed tomography

The advances in laboratory X-ray sources and detectors have allowed the progress and development of micro-CT. The process of CT imaging involves collection of projections (radiographies) from several hundreds of orientations (angles) of the X-ray intensity attenuated by the object of interest on an imaging device. Collected data (so-called sinograms) are then reconstructed using algorithms, such as filtered back-projection (also called FDK from the people who introduced it: Feldkamp–Davis–Kress) (Feldkamp et al. 1984), generating an image of the object cross-section. If the X-ray source is a cone-beam one (able of acquiring a $M \times N$ radiography, as opposed to a fan-beam type source that only acquires a $1 \times N$ radiography), then several slices are produced in a single scan, producing a 3D reconstructed image of the object. To reconstruct a reliable image, each projection should be acquired at stationary conditions; thus, it is essential for the object to be motionless at each orientation. This is not feasible in a

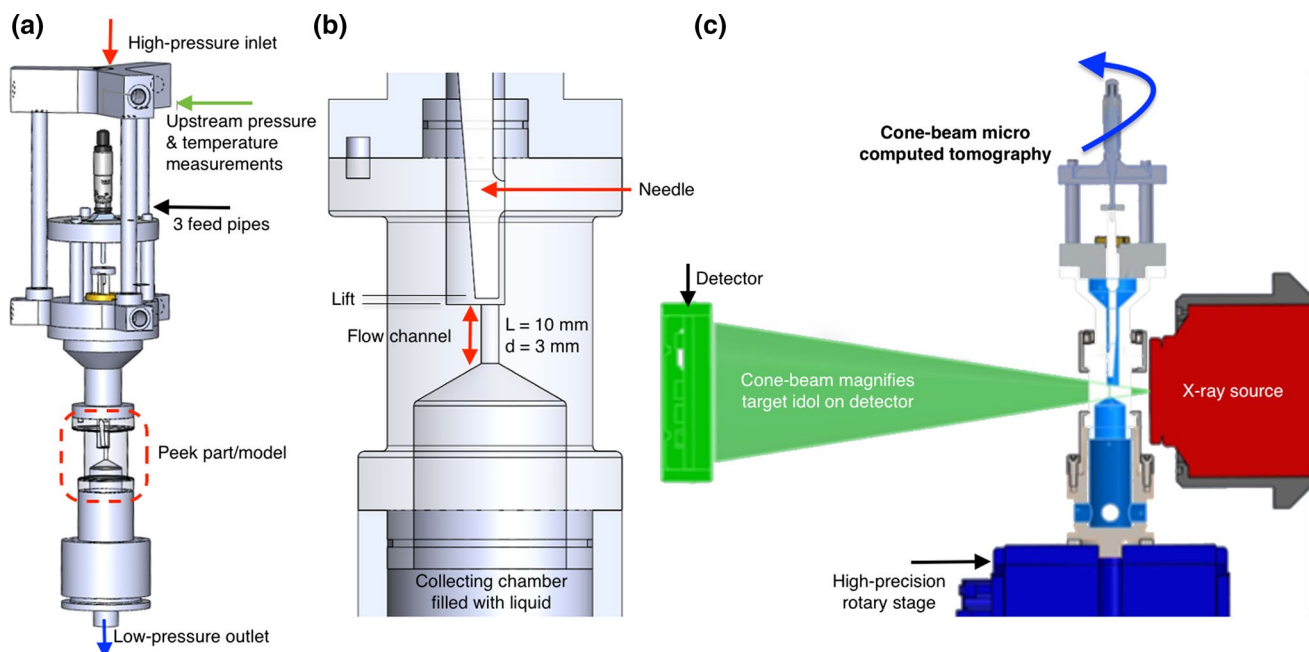


Fig. 1 **a** Overall test-rig set-up **b** flow channel model cross-section with dimensions and **c** tomography experimental set-up

Table 1 Range of experimental conditions

	Range of operation	Experimental conditions presented				
Needle lift (mm)	0.5, 1 and 2	0.5	1	1	1	2
P_{in} (bar)	10–60	30	42	17	45	25
P_{out} (bar)	5–20	9.7	13.5	7	18	10
Flow rate (l/min)	14–30	15.5	23.5	14.7	23.5	20
CN ^a	0.8–3.8	2.1	2.1	1.5	1.5	1.5
Re	30–67 k	36.5 k	55.5 k	34.6 k	55.5 k	47 k
C_d	0.5–0.78	0.52	0.66	0.7	0.7	0.78
Temp (°C)	40 ± 0.5					

$$^a \text{ Cavitation number: } CN = \frac{P_{inj} - P_{chamber}}{P_{chamber} - P_{vapour}}$$

transient multiphase flow environment, so each projection is acquired over a time scale that averages any signal fluctuation, which effectively results in averaging of the flow features observed. As shown in Ikeda et al. (1983), the result of reconstructed CT projections represents a time average of the varying quantities, when applied to dynamic flows; the latter is valid as long as the image acquisition time is much larger than the characteristic time scale of the variations.

The prototype micro-CT facility available at the University of Bergamo consists of a 160 kV @ 400 μ A open type cone-beam X-ray source, an air-bearing direct drive rotary stage and a 1944×1536 pixels flat panel CMOS detector characterised by a custom-matched scintillator plate in order to enhance the detection of low doses as used with low densities, such for the diesel fluid of interest. The X-ray facility is described in detail in Santini et al. (2013), where the validation of the technique for extraction and estimation of multiphase interfaces is also presented (Santini and Guilizzoni 2014; Santini et al. 2015). The spatial resolution has been adapted to obtain, in the reconstructed volume, an isotropic voxel size of 15 μ m. This voxel dimension has been considered adequate to picture the cavitation phenomena of interest. For an accurate three-dimensional reconstruction of the flow structures, tomographic projections were acquired over a full revolution of

the test-nozzle (360°) every 0.6° (600 projections). At each angular step, five projections were acquired and averaged to improve signal to noise ratio; therefore, the full scan time for each test case had been approximately 1 h, since a projection acquisition time of 1 s had been used. During acquisition, no beam filtration was applied to the incoming X-rays produced by the source that was set-up to 60 kV and 40.2 μ A. The gathered radiographies of the flow inside the injection hole were corrected for any detector defects and normalised against a nominal X-ray intensity that corresponds to attenuation of X-rays through air. Following the application of the logarithmic absorption law, appropriate filters were used to enhance the boundaries of different density materials. Examples for both the normalised and filtered radiographies are illustrated in Fig. 2b, c; for the purposes of this study and due to the total absence of metal parts in the X-ray field of view, only a frequency ramp filter was applied and the result was rendered adequate for the subsequent application of the selected reconstruction algorithm. Therefore, the back-projection algorithm (Feldkamp et al. 1984) was translated in a custom-developed routine, where all collected radiographies were assembled in order to reconstruct the three-dimensional image of the flow field. Figure 2a illustrates a schematic of the cone-beam computed tomography Cartesian systems; it is evident that the term “back-projection” refers to the process

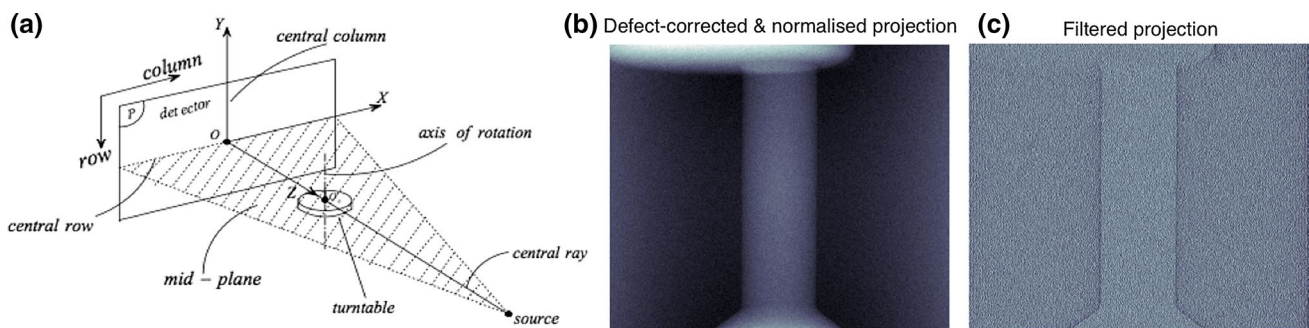


Fig. 2 **a** Schematic of cone-beam computed tomography Cartesian systems **b** normalised single radiography (projection) and **c** Ram-Lak filtered projection

of back-projecting the acquired image on the detector plane (matrix of rows and columns), back to the Cartesian system of the original object (labelled “turntable”). In brief, the advantage of a cone-beam X-ray system is summarised in its ability to collect two-dimensional radiographies (as opposed to one-dimensional radiographies of the fan-beam system) of a magnified idol of the object in question. To achieve this, the setup takes advantage of the cone-beam angle and the ratio of distances of source–detector and source–object that determines the magnification factor.

Finally, a known source of errors, when reconstructing X-ray CT images, are artefacts within the image. Common sources of artefacts are beam hardening, ring artefacts, and abrupt changes in density (Ketcham and Carlson 2001). Beam hardening is the most common artefact found in X-ray CT reconstructions that causes the edges of the scanned object to appear brighter than the centre, even for homogeneous materials. An effective way to reduce beam hardening that is more severe in metallic objects than plastics, is by filtering low-energy “soft” X-rays with metal filters. For this experimental campaign, no beam hardening filtration was planned mainly due to the absence of metallic parts and a possible reduction in the image contrast imposed by extra filtration. Instead, indirectly (by design), beam hardening was partly treated through the usage of beam filtration directly at the sample; i.e., the PEEK model acted as a beam filter surrounding the volume of interest (i.e. the injection hole), filtering the incoming X-rays before they reach the channel. Ring artefacts, in the reconstructed image, are caused by non-uniform response of adjacent detector elements to changes in X-ray energy. These errors can be minimised through proper calibration; however, the nature of tomographic reconstruction will promote even subtle differences in adjacent detector elements to ring artefacts. The measures taken by the authors to reduce ring artefacts are summarised in (1) using as input for the reconstruction the bright and dark images for proper correction of the unevenness of the detector values without the sample being present; (2) calculating as accurately as possible the detector offset and tilt parameters to compensate for the non-nominal scanning geometry and introduced the pointwise calibration for the reconstructed slices to diminish also this kind of artefact. Nevertheless, such artefacts have been observed and are visible in Figs. 7 and 8 along the channel centreline. Finally, abrupt changes in system density result in sharp changes in intensity signals that lead to streaks in the reconstructed image, due to approximations in the reconstructed algorithms. The best way to minimise streaking is by optimised system design to minimise sharp density differences in the imaging region. Test cases of the current investigation that suffered streaks due to abrupt changes in density were only the 0.5-mm needle lift cases, where the close vicinity of the metal needle to

the injection hole created some inevitable problems. However, in order to discard any source of ambiguity and errors, we discarded the first ~0.5 mm of the injection channel. Finally, it is essential to note that most of the known artefacts related to CT reconstructions are more pronounced in the case of metallic objects, as opposed to using softer materials, like plastic, that exhibit lower attenuation coefficients than metal.

2.3 Post-processing

Application of the filtered back-projection reconstruction process results in conversion of the intensity data in the sinogram files to CT numbers or CT values. These values correspond to the grey scale value in the resulting reconstructed image. It is important to highlight that during the CT reconstruction, the CT values usually map linearly to the effective attenuation coefficient of the material in each voxel (3D pixel) (2001). Hence, the variation in X-ray local attenuation is closely related to variations in local density (Du et al. 2008). This information is then used to determine local time-averaged phase fractions in a two-phase system.

Following the tomographic reconstruction of the flow channel, the obtained spatial X-ray attenuation coefficients are post-processed against two calibration sets in order to derive liquid fraction information per voxel; the post-processing procedure is described in Mitroglou et al. (2015) and a schematic of the procedure is illustrated in Fig. 3. In brief, the time-averaged liquid phase fraction in element (i, j) , equals the ratio of differences between the time-averaged CT value of the flowing system at location (i, j) , μ_{ij} , minus the time-averaged CT value of 0% liquid phase (μ_{ij}^{air}), over the difference of time-averaged CT values of the two calibration sets, μ_{ij}^{liq} and μ_{ij}^{air} . These correspond to time-averaged CT values of 100 and 0% liquid phase at location (i, j) , respectively. Finally, results refer to time-averaged liquid volume fraction information over the measurement period that is 1 hour, and the relevant error analysis showed that the followed post-processing procedure produced an error of ~5%. The latter is attributed to several facts, the most important being: the reconstruction technique, which is an approximate technique and the variation in X-ray intensity during a complete 360° acquisition.

Following the extraction of liquid volume fraction information, it is evident that the data refer to the complete scanned volume. An extra post-processing procedure was followed that is a common practice in the X-ray synchrotron experimental community; see selectively (Duke et al. 2015a, b; Kastengren and Powell 2014; Lin et al. 2012). In brief, exploiting the uniformity of the Cartesian three-dimensional grid, the projected void along the channel length is calculated by a summation of the product of vapour volume fraction at each location (i, j, k) multiplied by the corresponding voxel’s volume; the sum is then

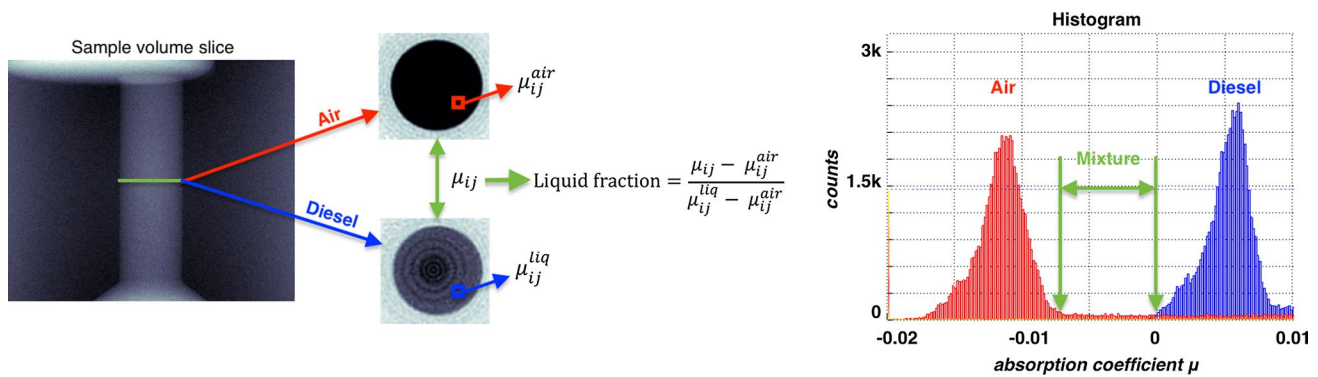


Fig. 3 Schematic of post-processing procedure followed to obtain liquid fraction of data sets, using the essential calibration sets

divided by the square of the cell grid size. The projected vapour volume fraction has length units and it effectively presents a line integral of the non-dimensional quantity $(1 - \alpha_{liq})$ supplementary to liquid volume fraction (Duke et al. 2014) calculated in the previous processing step (Fig. 3).

2.4 High-speed shadowgraphy

A second model (manufacturing tolerance of 20 μm) was manufactured from Perspex that allowed high-speed shadowgraphy to be performed. As mentioned in earlier paragraphs, flow visualisation suffers severe light extinction even at very low vapour volume fractions; however, it enables ultra-high-speed photography that provides qualitative information on cavitation vapour topology. In the current study, shadowgraphy images of selected test cases were acquired at 80 k frames per second. The collected images are then post-processed to extract statistical information on the topology of cavitation structures and their variations. The population used in this statistical analysis is 80 k images per test case, which corresponds to real flow time of 1 s. The derived mean and standard deviation images are presented alongside quantitative micro-CT measurements.

3 Results

The results presented in this section constitute a mix of quantitative X-ray time-averaged measurements and qualitative shadowgraphy statistical images. This helps the reader to complement time-averaged liquid volume fraction distributions inside the flow channel with ultra-fast images of the flow that capture the transient behaviour of the multi-phase flow system.

3.1 Flow pattern

Figure 4 is divided in two columns, illustrating high-speed shadowgraphy and quantitative X-ray time-averaged liquid

volume fraction measurements at the left- and right-hand-side columns, respectively. As seen in the instantaneous high-speed image at the top-left corner of Fig. 4, where cavitation structures are imaged in dark shades and liquid in lighter shades, the vapour cloud occupies mainly the bottom side of the channel. As the flow comes from the left-hand side, the asymmetry of the flow test-rig directs the flow to enter the orifice from the bottom side thus, vapour on this side is extended at larger lengths inside the channel; on the contrary, at the top channel side cavitation collapses at relatively shorter lengths. Statistical information extracted from the shadowgraphy images, as mean intensity and standard deviation maps (seen below the instantaneous image), illustrates a red-coloured area in the mean image, where cavitation is found to be present for the total duration of acquisition; on the contrary, the standard deviation image, having discarded the locations that exhibit zero variations, demonstrates the regions with high variability in intensity values throughout the test case. Three locations of transient behaviour inside the injection hole are identified from the standard deviation image; one (1) approximately at the top mid-length of the hole that is related to the extent of the top entry cavitation structures and the bulk of the void volume located below (diameter-wise) that area. The second (2) location is shortly upstream the exit of the hole and on the top half of the channel diameter, and it is related to detached bubble clouds that are seen to leave the main void and travel along the channel length. The third location (3) with increased deviation from the mean is at the vicinity of the entrance of the channel, where the transient string (or vortex) cavitation phenomenon is captured and illustrated in the contour plots. These structures are vortices that capture vapour (or gas) in their core, appear as thin dark tubes on a shadowgraphy image and have a lifetime of 25–50 μs . Moreover, the periodic detachment of vapour bubble clouds from the main cavity that give rise to increased variability in intensity values found in the standard deviation image is a bubble cloud shedding mechanism almost identical to the

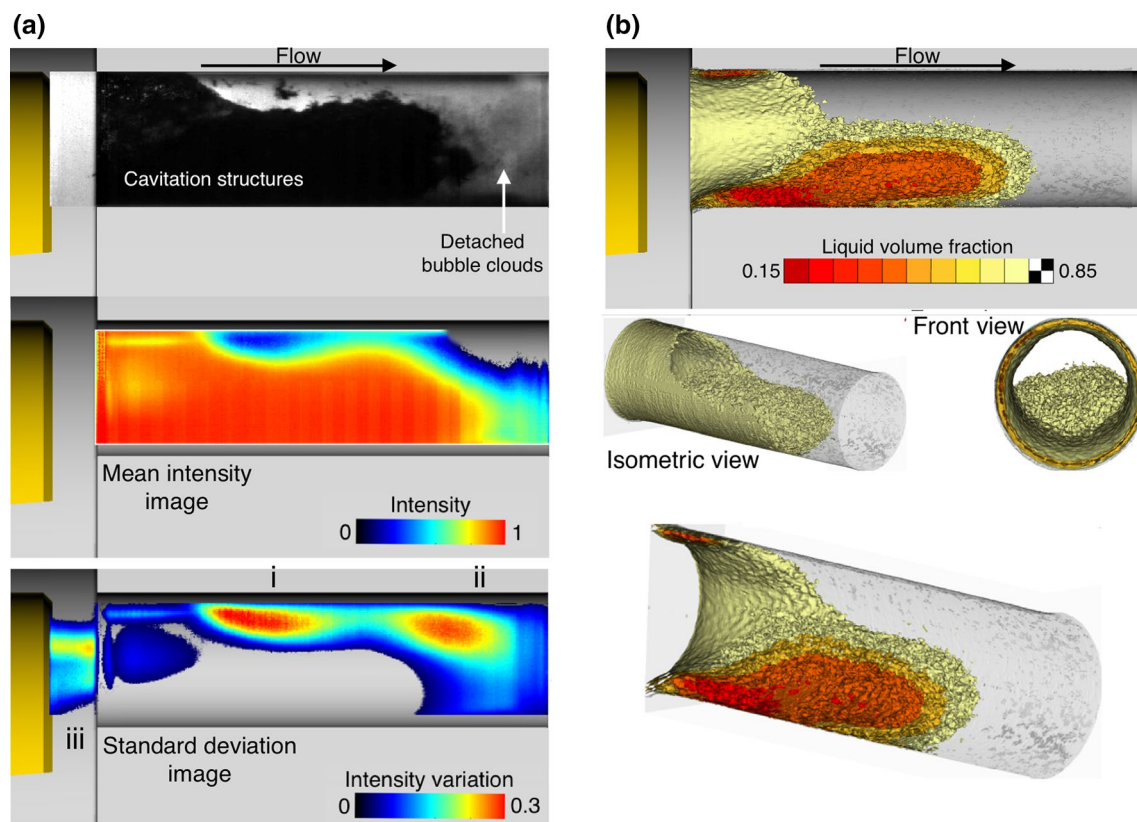


Fig. 4 **a** Instantaneous flow shadowgraphy image and corresponding mean and standard deviation images false-coloured according to pixel intensity values. **b** micro-CT measurements of liquid volume frac-

tion presented as side-view-cut iso-surfaces and isometric and front view images. Flow conditions are identical for **(a)** and **(b)** [$CN = 2.1$, $Re = 55.5$ k, $C_d = 0.66$ and needle lift of 1 mm]

one reported in hydrofoils, i.e., in Choi and Ceccio (2007), Coutier-Delgosha et al. (2006) and Sun et al. (2015).

Focusing only on the visualisation sample of Fig. 4a, an observer may come to a false-representation of cavitation that seems to entirely block the first half of the flow channel. However, observation of the micro-CT results on Fig. 4b, immediately corrects the wrong perception of the flow given previously. The two isometric view representations in Fig. 4b correspond to the complete channel, a cut at the symmetry plane as well as the front view of 80% liquid volume fraction. They demonstrate that cavitation starts as a ring, at the entrance of the nozzle hole, leaving the volume around the axis of the hole available to the liquid flow. As the nozzle model promotes asymmetric flow entry to the orifice, flow velocities and turbulence inside the channel differ from top to bottom. Thus, the cavitation cloud shapes accordingly, as seen at the top micro-CT image of Fig. 4b, where half of the channel is illustrated. Low values of liquid volume fraction are observed at the top of the channel; cavitation diminishes relatively quickly (almost at the first quarter of the hole length). Similar levels of liquid volume fraction at the bottom of the channel extend further inside the flow orifice up to almost 3/4 of its length.

A direct comparison of shadowgraphy versus micro-CT results is illustrated in Fig. 5, where the top row presents an instantaneous, a mean and a standard deviation image of the flow inside the channel at a low cavitation number (CN) of 1.5. At the bottom row of the same figure, micro-CT results of the exact flow conditions are presented as contour plot on the symmetry plane, liquid volume fraction iso-surfaces on half-channel and projected vapour volume fraction of the total depth of the channel. In brief, from top left to right, the instantaneous image illustrates a snapshot of all observed flow phenomena inside the flow channel like string cavitation and a detached bubble cloud; the mean image alongside presents a qualitative representation of the vapour cloud and the standard deviation image illustrates the locations with increased variability. On the bottom row, a contour plot of liquid volume fraction on the symmetry plane is displayed on the left, followed by a half-channel representation of liquid fraction iso-surfaces and the third image illustrates projected vapour volume fraction. While a plane-cut contour plot quantifies liquid volume fraction as low as 50%, for the presented conditions, cavitation extent does not look similar to an instantaneous flow image. This discrepancy between shadowgraphy qualitative data and

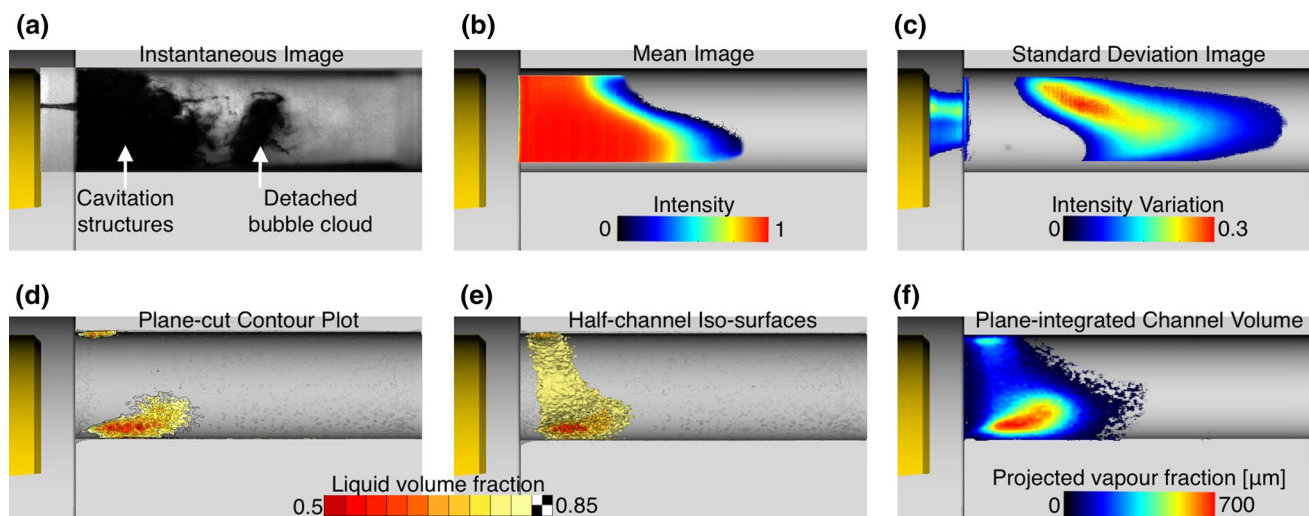


Fig. 5 Comparison of high-speed shadowgraphy images versus micro-CT liquid volume fraction. **a** Instantaneous shadowgraphy image; **b** mean cavitation image; **c** standard deviation images; **d** liq-

uid volume fraction on the mid-plane; **e** half-channel liquid fraction iso-surfaces; **f** plane-integrated channel volume vapour fraction contours [CN = 1.5, $Re = 55.5$ k, $C_d = 0.7$ at 1-mm needle lift]

micro-CT volume fraction measurements is not minimised even when comparing a half-channel representation with liquid volume fraction iso-surfaces; it is evident from the results that even a liquid volume fraction as high as marginally below 85% is able of blocking the light intensity, in the case of shadowgraphy. However, comparison of the plane-integrated micro-CT results to imaging data proves to be more realistic, as locations with projected vapour fraction marginally larger than $0 \mu\text{m}$ coincide with that locations of shadowgraphy images that exhibit minimum to zero intensity variability.

3.2 Liquid fraction measurements

Quantitative liquid volume fraction measurements can quantify the effect of various operating parameters on cavitation.

Initially, the effect of the needle valve lift is examined in Figs. 6 and 7. In detail, Fig. 6 illustrates a direct comparison of micro-CT data (top and middle rows) versus high-speed shadowgraphy (bottom row). As shown in Fig. 6, the needle valve distance to the orifice entrance varies from 2 to 1 mm; the latter has been selected as the nominal lift for the majority of the test cases. The two presented cases share a cavitation number of $CN = 1.5$ and a Reynolds number that varies between $Re = 47$ and 55 k, for the increased lift and the lower lift case, respectively. Given the expected negligible effect of marginal differences of the Reynolds number on cavitation structures (Mitroglou et al. 2016), it is evident that presented data are mainly affected by the change in needle valve lift. For the 2-mm needle lift value, the measurements show a confined vapour distribution, where liquid

volume fraction values are as high as 80%. As the needle valve lift is reduced to 1 mm (right-hand side of Fig. 6), the developed phenomena become more intense, compared to the high needle lift case. For the case of 1 mm lift, liquid volume fraction iso-surfaces denote that cavitation now extends almost up to one-third of the hole length and in the core of the created cavitation cloud, liquid volume fraction values are as low as 60%. Finally, interpretation of the high-speed shadowgraphy standard deviation images at the bottom row of Fig. 6 dictates that the higher the needle lift, the more the cavitation cloud instability inside the flow channel. This is clearly shown by the large red-coloured area that presents a variability of $\sim 30\%$ from the mean intensity values. However, the opposite trend is captured for the case of string cavitation visible at the vicinity of the hole entrance; the low needle lift of 1 mm shows increased variability compared to the high needle lift of 2 mm.

At even lower needle lifts than 1 mm, a similar trend is found and is depicted in Fig. 7, where the nominal lift of 1 mm is compared against the lowest tested lift of 0.5 mm. The flow conditions in both cases are similar sharing the same cavitation number of $CN = 2.1$ and $Re = 55$ k for the 1-mm lift case and $Re = 36$ k for the lowest lift case. This difference in Reynolds numbers is due to the low lift that inevitably limits the flow area available upstream the channel entrance to values lower than the channel's cross-sectional area. Nevertheless, the cavitation number of 2.1 causes extended cavitation in the 1-mm lift case, as shown by the contour plot on the channel's symmetry plane; however, as shown in the embedded front view image, there are still locations inside the channel that exhibit either negligible, or no cavitation at all. Despite the lower Reynolds

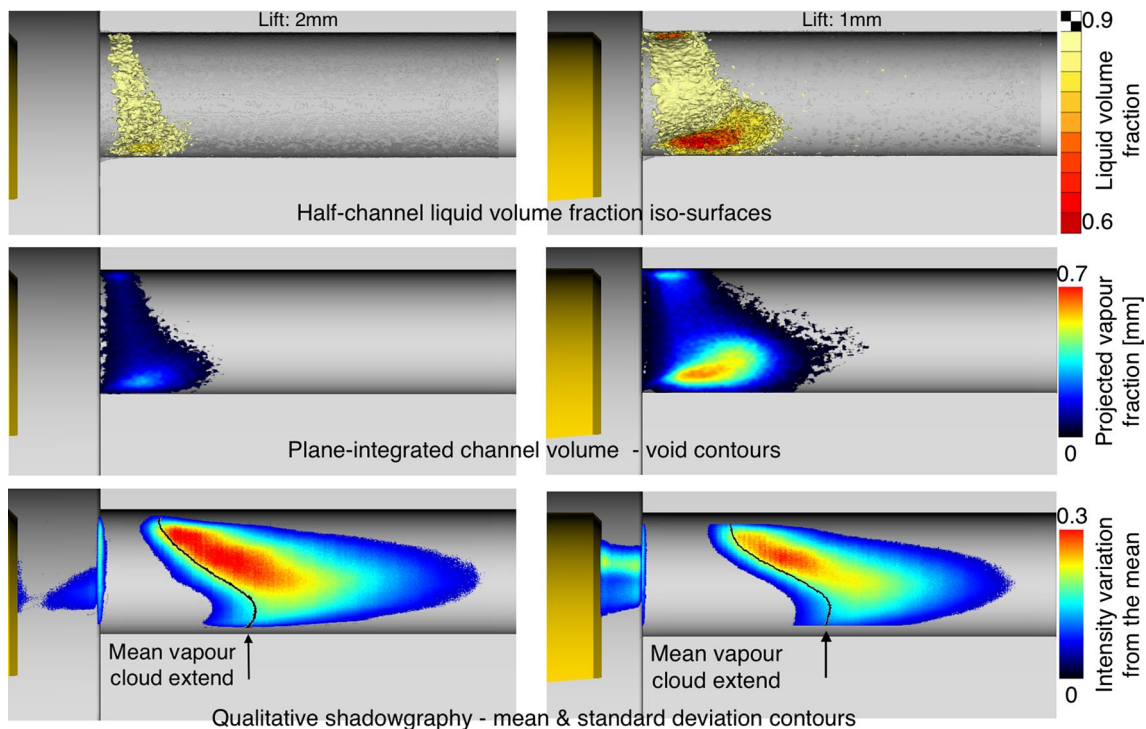


Fig. 6 Effect of needle lift position on vapour pockets presented as liquid fraction iso-surfaces for half the channel. Cavitation number is fixed at 1.5 and Reynolds number equals to 47 k for needle lift = 2 mm and 55.5 k for the low needle lift of 1 mm

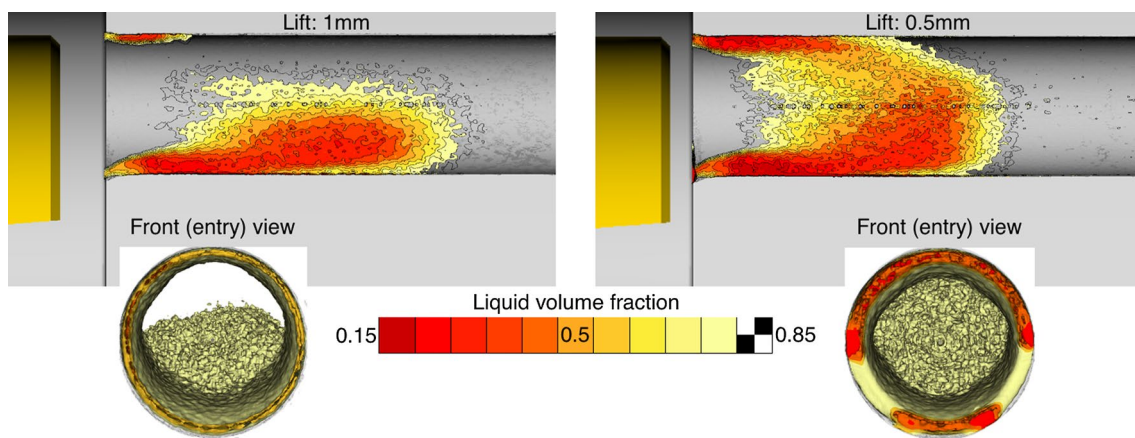


Fig. 7 Effect of needle lift position on vapour pockets presented as liquid fraction contours on the channel symmetry plane. Cavitation number is fixed at 2.1 and Reynolds number is 55.5 k for the high lift of 1 mm and 36.5 k for the low lift value of 0.5 mm

number for the lowest lift case of 0.5 mm, the flow picture on the symmetry plane is drastically different to the one of 1 mm lift. It is evident from both illustrated views of 0.5 mm lift that almost 1/3 of the channel length is occupied by liquid volume fraction ranging from 15 to 60%. Additionally, the area exhibiting extra low liquid volume fraction of ~15% is larger for the lowest lift case, compared to the basic lift of 1 mm. Finally, it has been established that needle valve lift has a pronounced effect on cavitation

structures, as it promotes turbulence, which, in turn, promotes cavitation. Unfortunately, the total channel blockage with vapour at the lowest needle lift prevented meaningful shadowgraphy data to be collected, as there was no light penetration through the channel due to increased vapour.

A direct comparison of the effect of cavitation number (CN) on vapour generation is illustrated in Fig. 8. At the nominal needle lift of 1 mm, Fig. 8a corresponds to $CN = 2.1$ and it presents, from top to bottom, micro-CT data in the form of

half-channel iso-surfaces, plane-integrated channel volume void fraction and hi-speed shadowgraphy standard deviation images; the same data representation is illustrated in Fig. 8b for the lower cavitation number of $CN = 1.5$. The Reynolds number for both cases is fixed at $Re = 55$ k. It is immediately evident that increasing CN has a significant effect on the cavitation cloud extent; in Fig. 8a, the vapour cloud extends up to 75% of the channel length and liquid fraction in its core is as low as 5%. Instead, in Fig. 8b, a limited extent of cavitation structures is shown and liquid volume fraction as low as 55%. The observed differences in vapour production inside the flow channel were expected, since the pressure difference across the injection hole, as denoted by CN , is mainly responsible for the initiation and development of geometric cavitation. However, what was unexpected in these illustrations is a slight vortex-like vapour shape that appears above the axis of symmetry of the channel at the left-hand side of the cavitation cloud of $CN = 2.1$ case (marked inside an ellipse). It resembles a string-like shape with its tip facing the hole entrance. This is the vicinity where cavitation strings have been recorded by high-speed shadowgraphy experiments as it is verified in the bottom row standard deviation images, where variability is indeed increased at the hole entrance vicinity. Of course, it is impossible for the time-averaged data of micro-CT to capture such a transient feature; however, the existence of the previously described shape may be closely related to

increased vorticity in that location, which may be adequate to promote string formation. Finally, the same structures exist also in the lower CN case of 1.5 (bottom image of Fig. 8b); however, their intensity and lifetime is not as pronounced as at higher CN .

Finally, Fig. 9 illustrates the effect of Reynolds number on cavitation development. At a fixed $CN = 1.5$ and needle lift of 1 mm, it is evident that an increase in Reynolds number from 35 k (Fig. 9a) to 55 k (Fig. 9b) has a marginal effect on vapour pockets inside the flow channel; increasing Re from 35 to 55 k only resulted in marginally lower liquid volume fraction measured in the core of the vapour cloud and in marginally larger channel volume occupied by the highest void fractions (middle set of images in Fig. 9), compared to $Re = 35$ k. It should be noted that the false colour scale for the Reynolds number comparison ranges from 0.6 to 0.9, as opposed to the left-hand side of Fig. 8, where it ranges from 0.15 to 0.85; hence, the different contour colours for the case of $CN = 1.5$ and $Re = 55$ k, which is identical in both columns of this figure. Finally, the transient behaviour of both cases is presented in the standard deviation shadowgraphy images (bottom row of Fig. 9), where low Reynolds number showed increased variability in cavitation cloud shapes inside the channel, while the high Reynolds number demonstrated increased string cavitation activity at the entrance of the hole.

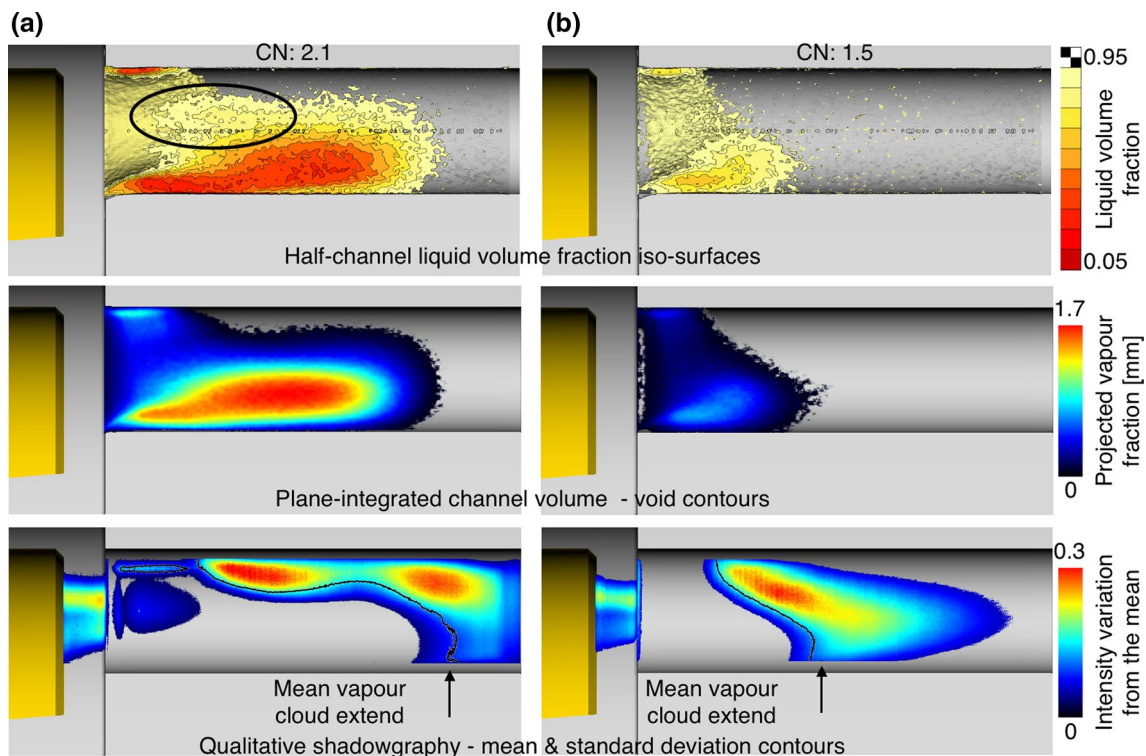


Fig. 8 Effect of cavitation number (CN) on vapour pockets at fixed needle lift of 1 mm and Re of 55 k; **a** $CN = 2.1$ and **b** $CN = 1.5$

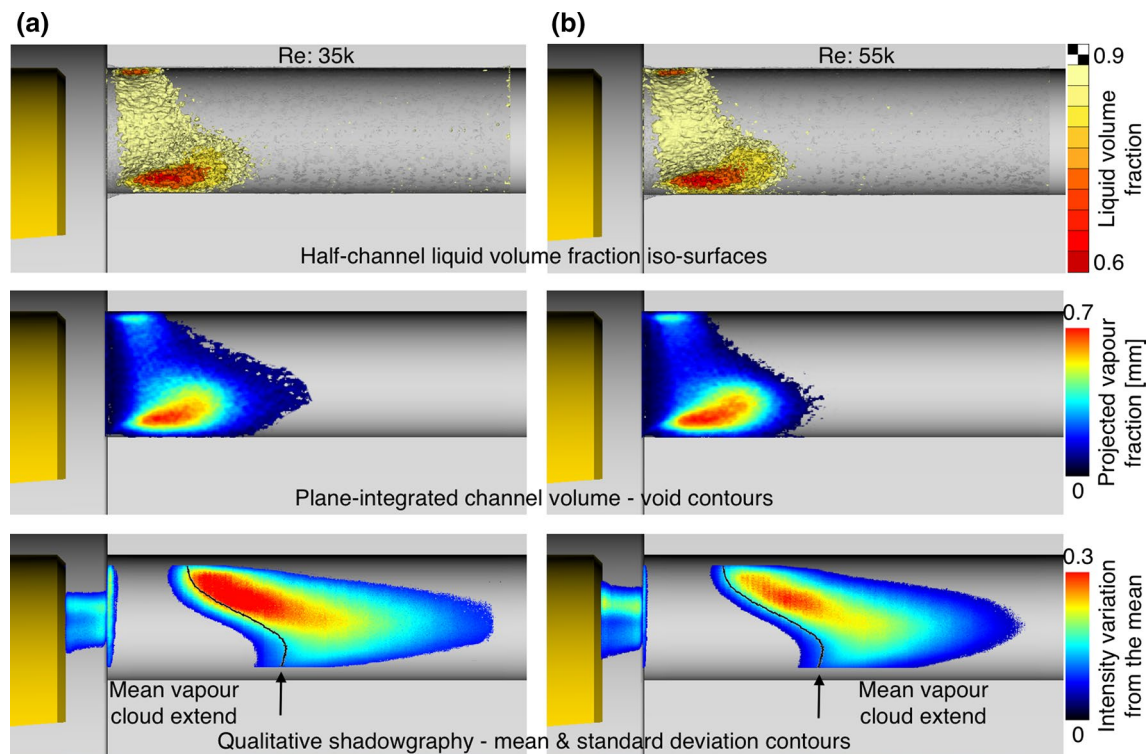


Fig. 9 Effect of Reynolds number on vapour pockets at a fixed lift of 1 mm and cavitation number of 1.5; **a** Re : 35 k and **b** Re : 55 k

4 Conclusions

The present study investigated the possibility of applying the micro-CT technique on highly transient cavitating diesel fuel flows and results appear promising in terms of time-averaged quantitative fuel vapour measurements. The technique produced results that compared seamlessly to the high-speed visualisation data, obtained from an identical transparent model. It has been established that a combination of both techniques is advantageous, as it provides a mix of average quantitative measurements and instantaneous qualitative images that provide valuable statistical information on the transient features of the flow field. The effect of flow parameters on cavitation structures has been quantified, and the expected results were observed. Needle lift valve was found to have a strong effect on vapour generation and vapour pocket extent inside the channel. Moreover, cavitation number effects on cavitation behaviour was examined and the expected results were confirmed. Finally, the effect of Reynolds number was investigated; however, the results do not show any significant change in cavitation vapour cloud behaviour.

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